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Lignocellulosic biomass feedstock: A benchmarking green resource for sustainable production of bioplastics

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ARTICLE INFO	ABSTRACT
Received : 25 November 2022	Presence of plastics in the surroundings is ubiquitous, as generation of plastics is
Revised : 14 March 2023	booming globally and it gets accumulated in oceans leading to deleterious
Accepted : 01 April 2023	impacts on marine life, public health and the surrounding environment. Owing
Available online: 17 August 2023	to its non-degradable nature, plastic particles remain in surroundings for extended periods which automatically facilitate its out spreading. Therefore, there is a need to shift to bio-based plastics, as bio-based green economy hinges
Key Words:	on sustainable employment of bioresources for generating a broad spectrum of
Biopolymer synthesis	products, biofuels, chemicals and bioplastics. Typically bioplastics are
Pre-treatment	synthesized from bio-based resources considered to contribute more to
Polyhydroxyalkanoates	sustainable production of plastic as a part of the circular economy. Bioplastics
Polylactic acid	are luring attention and growing as counterfeit material for petroleum-derived
Renewable feedstock	plastics owing to their biodegradability. Recently an engrossed interest has been
	burgeoning in producing drop-in polymers and new-fangled bioplastics by
	utilizing lignocellulosic feedstock. This paper reviews the enormous potential of lignocellulosic feedstock as a significant inedible substrate for bioplastic synthesis. Polyhydroxyalkanoates, polyurethanes, polylactic acid and starch- bioplastic are prevailing bio-based plastic comparably derived from lignocellulosic biomass. In forthcoming years bioplastic derived years' bioplastic derived from lignocellulose will loom as valuable material in numerous fields for an extensive range of cutting-edge applications.

Introduction

conquered human lives owing to their inexpensiveness, flexibility, versatility and exceptional thermal properties. Plastic is an indispensable artificial polymer that has surmounted contemporary societies. Accumulating plastic wrecks in marine areas dates back half a metric tons annually into the terrestrial environment century, with progress piling up on the ocean's as of 2016 (Rhodes, 2018). Plastic has numerous surface in the past 60 years. But even in one of the applications for multifarious utilizations and is a

Plastics have circumvented other polymers and most promising scenarios of the ultimate reduction of plastic waste in forthcoming years, plastic is aggregating and building up regularly in the environment. The projected global emanation of plastics in ocean lakes and rivers ranges from 9 to 23 million tons yearly, comparably 13 to 25 million

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distinguished counterfeit for diverse materials. Proclaimed global reports show that relatively 187 million tonnes of synthetic polymers based on petroleum are profusely generated annually and consequentially result in an enormous accumulation of plastic material, which induces environmental deterioration (Li et al., 2021). Plastic garbage makes up around 8% of the entire weight of municipal solid waste, which is 25% (Lau et al., 2020). Degradation of conventional plastics takes about 20-100 years in nature. It creates perilous problems, for instance, water pollution, air pollution and environmental contamination, which are further infuriated by the incineration of petroleum-based plastics as it discharges noxious gases into the atmosphere. Plastic pollution is extensively perceived as a principal environmental burden, peculiarly in aquatic ecosystems due to prolonged biophysical breakdown.Additionally, the presence of plastics in oceans manifests an alarming situation for marine organisms and affects them gigantically. Plastics consist of pernicious components such as phthalates, antimony trioxide, (BPA), and polyfluorinated bisphenol А compounds; they generally leach and cause adverse impacts on health and the environment. Plastics customarily end up in landfills with municipal solid waste due to inadequate waste management practices. There are elucidations required to solve the menacing problem of plastic waste, which has triggered the need to generate environment-friendly materials such as bioplastics. Bioplastics are innovative materials of this century and would be of immense relevance to the materials world. Bioplastic generation and usage will advance more in the forthcoming years; owing to this; these materials require careful evaluation for waste management and sustainability. Bioplastics are approaching imminent substitutes for petroleumbased plastics to diminish the detrimental environmental impacts and perilous health issues (Okolie et al., 2020). Several applications of bioplastics have been depicted in figure 1. Bioplastic fabrication by exploiting renewable feedstocks has been endorsed in former years for the generation of advanced bio-sourced plastics. Using renewable resources for bioplastic production has distinguished research interest in the past years as an expedient to mitigate and alleviate greenhouse gas emissions that are principally

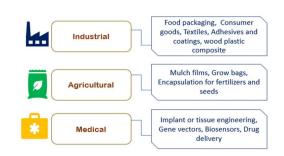


Figure 1: Plethora of applications of bioplastics

generated by fossil fuel burning, production and petrochemical-based fabrication of plastics. Because such materials might be used for the preservation of resources which automatically renders sustainability (Ahmad et al., 2018) among them, lignocellulosic feedstocks are an appealing alternative. Lignocellulosic feedstocks are specified non-edible plant components primarily composed of three building blocks (i.e. lignin, cellulose and hemicellulose) (Nanda et al., 2014). On average, lignin is (10-40%), cellulose (25-55%) and hemicellulose (11-50%) (Zhang et al., 2020). Lignocellulosic biomass (LCB) is principally categorized into forestry biomass (e.g. wood logs, sawdust bark etc.), energy crops (e.g. poplar, switchgrass, willow, elephant grass etc.) and crop residues (e.g. wheat straw, corn stover, rice straw, oat hall etc.) (Singh et al., 2020). LCB is a propitious feedstock for the feasible production of bioplastics owing to its non-seasonal opportunistic availability and socioeconomic advantages. Additionally, lignocellulosic feedstock being nonedible does not miens any competition to food crops, being contemplated as next-generation feedstocks (Nanda et al., 2018). Recently, numerous inedible resources such as bagasse, kraft pulp, corn stover, and switchgrass are being employed as lignocellulosic feedstock for a significant circular economy (Sherwood, 2020). This review highlights recent bioplastic overtures and bio-based polymer synthesis from lignocellulosic feedstocks. Fig. 2 depicts sustainable bioplastic production using LCB.

Present scenario of bioplastic production from lignocellulose

The aim of developing bio-based and eco-friendly polymers has tremendously increased in current years. LCB has enormous capability to produce bioplastics, and it is compelling because the Lignocellulosic biomass feedstock for sustainable production of bioplastics

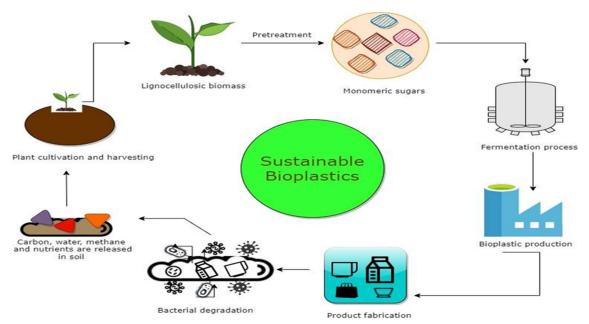


Figure 2: Sustainable production of bioplastics from LCB

generation of high-performing renewable materials is an indispensable factor for bio-based industries (Deepa et al., 2015). The usage of LCB for bioplastic generation faces confrontations, such as the high cost of production routes, and it signifies the necessity for technical advances and improvement in the field. In reported studies, it has been investigated that bioplastic production from organic waste and corn stover can typically cut down expenses (Kim et al., 2020). This interdisciplinary section of research is a remarkable amalgam of engineering and life science. It can offer and endeavour novel methodologies to redesign routes of biosynthesis for conversion of biomass; it will eventually lead to supreme economic and effective strategies to transform biomass into valuable commodities such as biopolymers (Galbe and Walberg, 2019). The recalcitrant nature of LCB is a primary heed in biorefinery industrial processes for bioplastic production and chemical transformation. In order to accomplish environmental and economic feasibility, it is necessary to use an adequate pretreatment method, which typically increments cellulose digestibility through disruption of the complex lignin-carbohydrate matrix; it also helps in increasing specific surface area and in reducing particle size ultimately, resulting in an extensive

recovery of sugar after the process of enzymatic hydrolysis. Pre-treated biomass could be saccharified using acid hydrolysis, by simultaneous saccharification and co-fermentation (SSCF) or by simultaneous saccharification and fermentation (SSF). Released monomeric sugars are directly fermented into biopolymers after the process of enzymatic hydrolysis. Required components are fermented by utilizing a broad range of microbes to produce several fragments that can be used for biopolymer production.

Pre-treatment of LCB for bioplastic production

LCB has a complex and heterogeneous composition, ultimately making it demanding for bioplastic production. In order to make LCB technically, environmentally, and economically feasible, there is a need to assimilate their production with different components. In the sector of bio-refineries, this includes techniques and several processes for the conversion and extraction of numerous products. Multifarious pre-treatment methods will be discussed in the next section.

Physical pre-treatment methods

Size reduction is a powerful method to escalate the receptibility of enzymes for hydrolysis. Hammer milling, chipping, cutting and grinding are the physical methods to curtail the particle size of biomass (Raj *et al.*, 2022), thereby immensely

increasing size, surface area pore and enzymatic decrystallizing biomass for high digestibility. Meanwhile, the final particle size totally depends on the kind of method used; chipping gives a particle size of 10-30mm, while milling and grinding provide a particle size of 0.2-2mm (Veluchamy et al., 2019). But the primary drawback of ball milling is that it consumes high energy and sometimes does not remove lignin content efficiently (Mankar et al., 2021). In a study to attempt the minimum energy consumption, wet desk milling (WDM) was used for the pre-treatment of rice straw, Hideno et al., (2009) found the energy requirement for 30 minutes (10 cycles of 3 min each) was 5.4 MJ/Kg. In contrast, the energy requirement during the dry ball milling method for the pre-treatment of rice straw under the same conditions was found to be 54 MJ/kg of biomass. The energy required for pre-treatment in the WDM process also depends on the kind of biomass feedstock (Da silva et al., 2010).

Another promising and encouraging thermomechanical method is extrusion; biomass is exposed to shear and heat with continuous mixing (Duque *et al.*, 2017). High temperature and pressure during the process modify the substrate's physical (defibrillation) and chemical structure; it boosts the availability of surface area and augments enzyme accessibility for expediting hydrolysis (Kumar *et al.*, 2020). Extrusion has been established as a comparable method for accustomed

methods, such as alkaline and acid treatments relating to hydrolysis efficiency. In a demonstrated study, a comparison of saccharification yields was established between extruded soybeans hulls with material pre-treated with alkali-acid and being extruded. Extrusion was found to be as competent as alkali, effectively superior to acidic pre-treatments, and improved saccharification by 132% (Yoo *et al.*, 2011).

Microwaves are nonionizing electromagnetic radiations having a wavelength range between 1mm to 1m, and these radiations selectively transfer energy to different substances (Huang et al., 2016). Microwave radiation disrupts recalcitrant units by triggering an explosion within the particles in the given material (Mankar et al., 2021). Microwaves have captured comprehensive attention in diligent biorefinery applications for the treatment of LCB, being a thermal process. And in the last three decades, the utilization of microwaves in the pretreatment processes of LCB has deliberately moved from the laboratory to pilot scale studies (Li et al., 2016). Heating by microwave distinguishably enhances the enzymatic saccharification process by fibre fragmentation and swelling (Diaz et al., 2015) by virtue of accelerated hasty and uniform heating of LCB particles. Plant fibres remain intact, and approximately no effect can be seen in plant fibres when pre-treated with microwaves under a temperature equivalent to 100 °C (Chen et al., 2017).

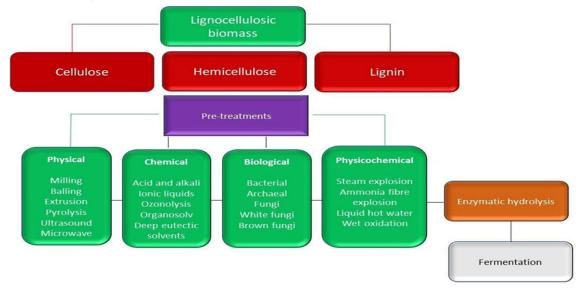


Figure 3: Different pretreatment approaches for LCB

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Alternatively, LCB is grounded into minuscule particles in traditional heating pre-treatment methods to avoid a temperature gradient. Then high-pressure steam injection and heat conduction are used for heating; it might degrade the hemicellulose in humic acid or furfural and therefore afflicts the sugar recovery (Li *et al.*, 2016). Fig. 3 shows several pre-treatment approaches.

Chemical pre-treatment methods

An array of distinct chemical methods are used for the pre-treatment of LCB, including organosolv, kraft pulping, ionic liquid and dilute acid etc. Mentioned pre-treatment methods have compellingly proven as an adequate and effective method for a broad range of lignocellulosic feedstocks (Tu and Hallett, 2019).LCB acid treatment is primarily accustomed to eliminate hemicellulose. Acid pre-treatment results in enhanced receptivity of enzymes towards cellulose; generally, phosphoric acid, acetic acid, and sulphuric acid are used for improved pre-treatment (Rezania et al., 2020). In dilute acid pre-treatment, LCB is treated through the action of hydrolysis and solubilization of hemicellulose and acid-catalyzed depolymerization of the lignin. Moreover, the type of acid used and its concentration can affect solubilized lignin's condensation (Hendricks and Zeeman, 2009). Two different ways could achieve acid pre-treatment - concentrated acid (30-70%) treatment at approximately lower temperatures and treatment at relatively dilute acid higher temperatures (Den et al., 2018). Both the mentioned approaches have their own leverage and impediments, In dilute acid treatment minimum amount of acid is used, but the needful energy requirement for the process is ultimately higher. On the contrary, meagre energy is consumed in treatment with concentrated acid, but it relatively results in higher acidity, which brings about the generation of fermentation inhibitor (5hydroxymethylfurfural). These inhibitors severely affect fermenter microorganisms by breaking down DNA and reducing RNA synthesis, which automatically hinders enzymatic activity (Woiciechowski et al., 2020). On the other hand, pre-treatment includes hydroxides of alkali calcium, sodium, ammonium, and potassium, amid pre-treatment bond cleavage (ester,alkyl-aryl, aryl-

ether) occurs, and uronic acid and acetyl groups are subsequently removed from hemicellulose and lignin (Kumar et al., 2020), and it results in improved access of enzymes towards cellulose thus helps in efficient fermentation of sugars(Cheah et al., 2020). In an investigated study, alkali-catalyzed hot water pre-treatment was performed at 170 °C, and it resulted in the alteration of present recalcitrants in bamboo biomass and produced 30.9% reducing sugars. In a reported study, pine poplar wood treated with sodium carbonate (NA₂CO₃) and NaOH(sodium hydroxide) at a temperature of 93°C, it adeptly dissolved hemicellulose and lignin content and generated 69.3% glucose (Bay et al., 2020). Furthermore, ammonia or CO₂ explosions and ozonolysis are effective alternative pre-treatment methods. Biological pre-treatments are usually innocuous and require low energy, and do not generally generate inhibitors for the downstreaming processes (Tu and Hallett, 2019). Microorganisms such as bacteria and fungi are utilized in degrading LCB to macromonomers by hydrolyzing cellulose or depolymerizing lignin (Chen et al., 2017)

Cellulose conversion routes for bioplastics production

Cellulose is extracted from LCB and practised for bioplastic production (Govil *et al.*, 2020). The ultimate amount of cellulose content relies on the source from which it has come. Conversion of cellulose into bioplastic composites includes lignin and hemicellulose removal, cellulose extraction and surface modifications (Reshmy *et al.*, 2021).

Hemicellulose removal and delignification

Generally, the removal of lignin includes high pressure and temperature, the occurrence of developmental processes at lower temperatures promptly removes the lignin, and simple recovery of chemicals becomes difficult (Yang et al., 2019). In the delignification process, lignin is isolated from biomass, and some part of hemicellulose also gets removed. Delignification is imposed using hydrogen peroxide, sodium chlorite and oxygen. Delignification results in the degradation of lignin content, transfer of it into a liquid medium and consequentially, proper of lignin by washing. elimination Delignification does not selectively remove lignin; therefore, some quantity of cellulose and hemicellulose is eliminated altogether (Reshmy et al., 2021).

Cellulose extraction and surface modification

Highly purified cellulose in different forms has been extracted by utilizing several processes relatively depending on the source and type of pretreatments (Mondal, 2017). Various methods such as pulping ball milling, microfluidization and practised homogenization are for cellulose extraction from LCB. Extracted pulp through these techniques can be further chemically and mechanically treated for liberating cellulose. Highpressure homogenizing techniques are used for refining to get the defibrillated cellulose in the nano range (Kargarzadeh et al., 2017). Combined force technique aids in high-pressure immense defibrillation and results in the generation of nanocellulose. The kraft process is a supreme chemical pulping method, in this method, lignin is dissolved using HO₃S⁻ and H₂SO₄ (Khalil et al., 2012). Another cellulose extraction method is steam explosion; this LCB is treated with several chemicals at high-pressure steam for a precise interval of time, followed by abrupt steam discharge. Due to the abrupt release of pressure, the extracted cellulose will be having high aspect ratio and size of particles in the nano range (De Moraes et al., 2013).

Cellulose has hydrophilic nature to boost its solubility and processibility; some surface modifications are needed, and various methods are being used for this purpose (Yoo and youngblood, 2016). Surface modification methods include surfactants and graft copolymerization (Rahman and Putra, 2019) and surface derivatization (Kargarzadeh et al., 2017). A graft polymer primarily consists of branches of a particular polymer being attached to the backbone of other polymers; typically, graft polymerization is of specific interest because of its adaptability in creating an extensive range of functional groups on the surface since it allows the combination of required properties of two or more polymers into an individual unit Acetylation was found to improve transparency, and thermal degradation contrastingly decreases the hygroscopicity of biocomposites of cellulose without even intruding the microfibrillar morphology (Ahmad et al., 2015). Owing to its defined structure, modifications can be made in cellulose in numerous ways; presence of hydroxyl groups in the chain offers many potential capabilities and the way in which cellulose will be

affected ultimately depends on the conditions and chemicals applied (Rol et al.. 2019). Carboxymethlation of cellulose generates extensively pure water-soluble cellulose derivatives being applicable primarily as ophthalmic solutions. Various novel enzymes have been substantially tested, such as laccases, hemicellulases and lytic polysaccharide monooxygenases (LPMO); these enzymes promote and improve fibrillation by improving access to cellulose to cellulase (Rodríguez-Zúñiga et al., 2015). In a study, an epoxy modification was done by surface modification of fibrils of cellulose through the of oxidation using cerium process (IV) consequential follow-up by grafting with glycidyl methacrylate (Oliveira et al., 2017). Bioplastics incorporated with cellulose have exceptional mechanical strength. They can be produced from the suspension of nanocellulose by practising several film-forming methods such as extrusion or blow molding.

LCB bioconversion to biodegradable and recyclable biopolymers

Polyhydroxyalkanoates (PHAs)

PHAs are polyesters and both biocompatible and biodegradable nature, consisting in of hydroxyalkanoic acids. Numerous bacterial species extensively synthesize them as a reserve material for carbon and energy. Synthesis of PHAs in bacterial cells occurs in unfavourable conditions like surplus carbon with environmental stress of essential growth nutrients such as phosphate, nitrogen or oxygen limitations (Annamalai and Sivakumar, 2016). PHAs have loomed and emerged as an excellent polymer for the corrective solution to the problem of plastic waste. PHAs are biodegradable in the marine environment and soil, forming methane, carbon dioxide, biomass and water as by-products after efficient decomposition (Chalermthai et al., 2021; Jadaun et al., 2022).

Additionally, PHAs classically represent those value-added products which are generated from renewable feedstocks such as LCB by utilizing microorganisms and pose comparable properties to petroleum-based polymers (Mannina *et al.*, 2019). Numerous strategies to produce PHAs from LCB have been developed and demonstrated based on the bacteria used or which LCB should be used (hemicellulose-rich or cellulose-rich) (Moorkoth and Nampoothiri, 2016). Various *Bacillus* sp. has

the potential to produce poly(3-hydroxybutyrate) [P(3HB)], a class of PHAs, from LCB without pretreatment, i.e. mango peels (Gowda and Shivkumar, 2014) and oil palm trunk sap (Lokesh et al., 2012) were utilized as a primary carbon source to produce [P(3HB)] in *B. thuringienis* and *B. megaterium* with a concentration of 4.03 g/L and 3.28 g/L respectively. However, detoxification and pretreatment are required in most cases. Over time, several methods have been advanced and developed for the pre-treatment of LCB s and to depose the inhibiting compounds for the efficient and adequate usage of lignocellulosic feedstock. Sugarcane bagasse, a cellulose-rich biomass, was effectively detoxified and pre-treated with acid to form sugarcane bagasse hydrolysate, it was utilized as a substrate to produce P(3HB) with an achieved 4.4 g/L and 2.73 g/L concentration of in Burkholderia cepacia and Burkholderia sacchari strains. (Silva et al., 2007). Another reported study demonstrated and established an integrated pretreatment process, AFEX (Ammonia fibre expansion), followed by enzymatic hydrolysis of hemicellulose and cellulose fractions to prepare wheat straw hydrolysate, B.sacchari potentially produced P(3HB) with a final titer of 105g/L by utilizing a feedstock that primarily consisted

xylose, arabinose and glucose in fed-batch 2014).PHA fermentation (Ces[']ario et al., copolymers production, counting natural and nonnatural PHAs, in addition to P(3HB), is another compelling research area. At first, numerous LCBs, such as sugarcane bagasse, rubber wood, cassava stalk and sorghum stalk, were investigated and tested for mixed microbial fermentation as a feedstock for the production of PHA after being given pressurized hot water treatment. Physical treatments given to feedstocks efficiently increase saccharification with the distinguished recovery of sugar yields of 178.0 mg/g of xylose and 438.7 mg/g of glucose in rubber wood. Microbial principally fermentation, including Alphaproteobacteria and Bacteroidia classes, culminated in the production of poly(3hydroxybutyrate-co-3-hydroxyvalerate) [P(3HB-co-3HV)] (Yan et al., 2021). Using the same microbial classes to produce P(3HB-co-3HV.), rubber wood hydrolysates were also investigated. Primary PHA accumulating strains belonging to the Bacteroidia and Alphaproteobacteria classes were successfully screened by adding xylose to rubber wood hydrolysate as a co-substrate with final PHA content of 43.6% of dried cell weight (Li et al., 2022). Table 1 is displaying production of PHA copolymers using LCB

Lignocellulosic feedstock	PHA Conc. (g/L)	% PHA accumulation (w/w)	Microbe used	PHA copolymer	References
Barley biomass hydrolysate	1.8	54	Ralstonia eutropha 5119	PHBV	Bhatia <i>et al.</i> , 2018
Grass biomass hydrolysates	0.3	33	Pseudomonas strains	MCL-PHA	Davis <i>et al.</i> , 2013
Liquefied wood hydrolysates	60.5	NA	Cupriavidus necator	PHBV	Koller <i>et al.</i> , 2015
Sawdust hydrolysates	0.3	78	Brevundimonas vesicularis and Sphingopyxis macrogoltabida	MCL-PHA	Silva <i>et al.</i> , 2007
Miscanthus biomass hydrolysate	2.0	44	Ralstonia eutropha 5119	PHBV	Bhatia <i>et al.</i> , 2018
Pine biomass hydrolysate	1.7	63	Ralstonia eutropha 5119	PHBV	Bhatia <i>et al.</i> , 2018
Rice bran and corn starch hydrolysates PHBV - Poly (3-bydroxybuty	77.8	55.6	Haloferax mediterranei	PHBV	Matsumoto <i>et al.</i> , 2011

 Table 1: PHA copolymer production from LCB (Govil et al., 2020)

PHBV - Poly (3-hydroxybutyric acid-co-3-hydroxyvaleric acid). MCL-PHA - Medium chain length PHA.

MCL-PHA - Medium chain length NA - Not available.

Polylactic acid (PLA)

Lactic acid (LA) is a polymerized chemical that could be utilized to produce biodegradable LA polymers using biotechnology on waste and agricultural residues (Djukić-Vuković et al., 2019). It has extensive usage in food, pharmaceutical and cosmetic industries as a preservative as it retards the growth of pathogens (Komesu et al., 2017). Still, the crucial application of LA is its usage in the processing and synthesis of polylactic acid (PLA), a significant biocompatible plastic currently in use. Biotechnological practices predominantly prevailed production and synthesis of LA to possibly obtain optically pure LA enantiomers by selecting a suitable strain which can be efficiently grown on renewable feedstocks, resulting in high productivity and purity (Lunelli et al., 2010). Commercially available PLA is generated by ring-opening polymerization and polycondensation (Garlotta et al., 2001), PLAs chirality is controlled by tuning the optical activity and dissemination of LA units in the polymer backbone; it enhances final polymer performance. Currently, sugar beet, sugarcane and corn starch are used as raw materials for the production of LA on a global scale. Profound research is going on PLA resin production on a lab scale using second-generation feedstock such as wheat straw bagasse, wood chips and corn stovers, striving to accomplish comparable qualities, challenges and solutions relevant to increase competitiveness sustainability and of LA production on agricultural residues and wastes. The fermentation of monomeric sugar generates biobased lactic acid, and hydrolysis of LCB is a luring way to the production of lactic acid. PLA being thermoplastic, can be easily transformed into different end products using numerous industrial techniques such as blow molding, fibre extrusion, film extrusion and injection molding; PLA's processing temperature is low in contrast to conventional thermoplastics. Numerous strains, such as Bacillus coagulans, can metabolize hexose and pentose to LA in an effective way. In a study, LA was synthesized from Beachwood and pine being organosolv pretreated, cellulose-rich solids were subsequently fractionated and simultaneously employed saccharification and fermentation using Lactobacillus delbrueckii subsp. in batch mode, and the final yield reported was 62g/L⁻¹ (Karnaouri et al., 2020). The polymerization of LA could be

carried out through either ring-opening polymerization or direct condensation polymerization (Lopes et al., 2014). Reactions in direct condensation require probably high temperature, an extended reaction time and low pressure for producing PLA of high molecular weight. On the contrary, ring-opening polymerization could be carried out at relatively low temperatures and requires a meagre reaction time. PLA being made from direct condensation generally has low molecular weight with indigent mechanical properties, while ring-openingproduced PLA has high molecular weight through heating in the presence of the catalyst, stannous octoate under Vaccum (Singla et al., 2012). In recent times several PLA-based technologies are imminently emerging expeditiously for the advances in developing green material procured by making blends with polymers and reinforced fibres like starch and cellulose with enhanced mechanical, chemical, and biological properties in accordance with the required application. List of various lignocellulosic feedstocks is given in Table 2 that could be used for producing bioplastics.

Bio-ethylene

Polyethylene (PE) is an aliphatic polyolefin generated by the polymerization of ethylene and conjointly impersonates more than 30% of the plastic market on a global scale (Hutley and Ouederni, 2016). And presently produced from natural gas or crude petroleum by employing steam cracking using numerous metal catalysts at a temperature of 750-850 °C. In spite of that, biobased-polyehtylene can be produced from secondgeneration ethanol generated in cellulosic biorefineries (Raj et al., 2022). Bioethylene is a chemically indistinguishable substitute for ethylene we get from petrochemicals. Bioethanol is produced from well-developed routes such as fermentation and hydrolysis of sugarcane and corn feedstocks. The ultimate production cost of bioethylene depends on bioethanol production, which shows the importance of the origin of bioethanol in the process. The technology used to convert ethanol to ethylene is well-established and commercially available; bio-polyethylene(bio PE) is a newly developed bioplastic being prepared and produced from ethanol extracted through solid-state fermentation of LCB (Reshmy et al., 2021).

Bioplastic	Lignocellulosi c feedstock	Specified condition	Microorganism used	Titer (g/l)	Reference
	Rice husk	Alkali pre-treatment given; Batch fermentation with supplementary urea	Burkholderia cepacia USM	2.35	Heng et al., 2017
	Corn stover	Combined acid and alkali pre- treatment; fed-batch fermentation using lignin	Pseudomonas putida KT2440	1.0	Sindhu et al., 2013
PHAs	Lignin	Fed-batch using lignin-abundant black liquor; obtained from alkaline pretreated sugarcane bagasse	Pseudomonas monteilii	0.24	Unrean <i>et al.</i> , 2021
PLA	Sugarcane bagasse	Acid pre-treatment; furfural- supplemented pre-culture	Bacillus coagulans	75.9	Van der Pol <i>et al.,</i> 2016
	Pulp residues	Fed batch SSF; pH neutralized with CaCO ₃	Bacillus coagulans	110	Zhou et al., 2016
	Sugarcane bagasse	Acid and steam explosion treatment; pH adjustment using NaOH	Lactobacillus pentosus	72.8	Unrean, 2018

 Table 2: Production of PHA and PLA using LCB (Kawaguchi et al., 2022)

Numerous commercial stakeholders, like SABIC (Netherlands), Braskem (Brazil) and Ineos (bionaphtha from UPM Biofuels) are currently producing bio HDPE, bio-PE and bio-LDPE from bioethanol, being derived from sugarcane (Raj et al., 2022). Moreover, advances in bioethanolproducing technologies are highly alluring, as they are a drop-in equivalent to petroleum-based polyethylene, bio-PE also displayed effective applications as being used ad epoxy resins as a substitute to petroleum-based processes (Delgadoaguliar et al., 2017). In a study bio-PE from sugarcane ethanol was synthesized for the purpose of biocomposite reinforcement application; it improved tensile and mechanical strength (Castro et al., 2017). Consequentially unified synthesis of C2 molecules from relatively bountiful renewable feedstock has acquired a massive interest in substituting synthetic plastics in biorefineries.

Polyglycolic acid (PGA)

It is an integral biopolymer owing to its biodegradable nature and mechanical properties which offers numerous applications of this biopolymer in the medical and renewable industries (Budak *et al.*, 2020). Glycolic acid (monomer of PGA) is relatively small alpha-hydroxy acid which consists of alcohol and carboxyl groups. PGA is produced petrochemically from formaldehyde and CO by utilizing several acid catalysts; it is an aliphatic ester of glycolic acid. Although it can also be obtained from renewable resources (sugarcane, sugar beets etc.), the worldwide market of glycolic acid will exceed from \$160 million in 2015 to an

estimated \$415 million by 2030 (Jem and Tan, 2020). Generally, PGA could be synthesized via two methods, first one is Poly-Condensation of glycolic acid and the one is Ring-Opening Polymerization of glycolide. Precursors of glycolic acid can be generated from renewable resources (grapes, cantaloupe, sugar beets and sugar cane) via biotechnological approaches by using genetically modified strains like E. coli and Corynebacterium glutamicum (Salusajarvi et al., 2019). Gokturk et al., (2015) optimized copolymerization conditions for the conversion of C1 feedstocks into formaldehyde and CO into PGA through cationic alternating copolymerization and ultimate results gave 92% yield of PGA with extensive crystallinity and high melting point (192°C), triflic acid was being used as catalyst. The presented method constituted a simple, effective and economical approach for the purpose of synthesizing PGA directly from C1 feedstocks, which are derived potentially from biomass. VTT research centre demonstrated the formation of glycolic acid using natural feedstocks i.e., sugar hydrolysate by the fermentation of sugars using constructed engineered yeast strains (Gadda et al., 2014). A number of blends can be prepared using PGA, PLA, PHAs and cellulose, in a study PGA-PLA polymer blend was prepared for particular uses in drug delivery and tissue scaffolds applications (Salusajarvi et al., 2019).

Polyurethanes (PUs)

PUs are generated from condensation polymerizations between polyols and isocyanates,

which are one of the most versatile and flexible polymer families. Presently, isocyanates and polyols together are extensively petroleum-derived; in recent years, comprehensive research interest has developed in generating polyols and PUs from renewable bioresources (Tenorio-alfonso et al., 2020). Being the most plentiful biomass in the world, LCB has enormous potential to be used as feedstock for the production of polyols and PUs as it contains hydroxyl groups (Malani, 2021). LCB acts as an economical substitute for the development of PUs. Conversion of LCB into liquid polyols for PU applications includes acid- or base-catalyzed atmospheric liquefaction processes using polyhydric alcohols as liquefaction solvents, and derived polyols could be further used to prepare several PU products like film, foams and adhesives. And eventual properties of these biomass-derived polyols extensively depend on the characteristics of the biomass being used and liquefaction conditions. Various diverse LCBs, including crop residues, wood and biorefinery byproducts examined for PUs and polyols production. LCB has solid nature; hence its chemical modification is essential to change LCB into liquid polyols for the generation of PUs. For optimized mechanical properties of PUs, it is necessary to incorporate versatile aliphatic polyols with tough and rigid lignin polyols (Kuranska et al., 2013). The ultimate mechanical properties of PUs largely depend on the relative content of lignin and its nature. Organosolv lignin (15-25 W%) in nonmodified forms generates quality PUs on the other hand, large quantities of lignin accompany brittle PUs. Lignin fragments having low molecular weight amalgamated with flexible polyols such as glycerol and polyethylene glycol via enzymatic with consequentially following hydrolysis mechanical treatments In a study conducted by Araujo and Pasa (2003), they used guaiacylhaving syringyl-based lignin residual polysaccharides obtained from Eucalyptus tar distillation, and prepared PUs using different amount of hydroxyl-terminated polybutadiene.

Challenges and future prospects

The abundant availability of LCB composed it an economical source for fabricating biobased polymers using innovative biotechnological avenues. Nonetheless, commercial feasibility is still defined by virtue of the huge cost of transportation,

curtailed pre-treatment efficiency, extensive chemical input and enzyme requirement demand. (Hassan et al., 2019). In the world's bioplastic market, the contribution and participation of LCBderived bioplastic are flat due to lower prices of crude oil. The approach of circular bioeconomy should be contemplated for the valorization of a variety of by-products from a specific biorefinery process. For instance, a pilot plant in cellulose biorefinery might be used for the production of the biodegradable polymer such as PLA and PHA from monomeric sugars. In the same way, ethanol being generated in the cellulosic biorefinery may be integrated with catalytic conversion techniques for the production of biological origin Bio-PE and PET (Rosales-Calderon, and Arantes 2019). However, recyclable bioplastic has comparable attributes to petroleum-based plastics, but worldwide acquiescence of these biobased plastics is still restricted. Presently, maximum bioplastics are being derived from monomeric sugars generated starch-based feedstocks: the apparent from complexity of LCB is its recalcitrant nature and inaccessibility to combined LCB to recyclable plastic process are primary limitations in its commercial evolution. Additionally, the maximum quantity of sugar titer after enzymatic hydrolysis and the requirement of well-fermenting microbial strains to produce bioplastic monomers are the prime tailbacks in LCB-based plastic manufacturing industries. The cost of feedstock plays an important factor, which significantly depends on harvesting methods, land use, and supply chain; therefore, a careful, perceptive understanding of all the factors would enormously contribute to bioprocess economics. However, numerous parameters like hydrolysis, pre-treatment and fermentation have been well investigated and documented in the literature though cost reduction of unified units at the commercial level requires evaluation.

Out of the total overall operational cost, 25-30% only accounts for processes of sugar extraction for bioplastic generation from LCB. Therefore a cocktail of development of in-situ, economic enzymes would be significant for the bioplastic industry. And on a general basis, the government must strengthen the effective implementation of policies related to biobased resources and should promote the usage of bioplastics instead of

synthetic plastic for daily routine applications. Although recycling compostable and biodegradable plastics is technically possible, however presently, <1% of bioplastics is being recycled due to nonof adequate labelling availability European standards of bioplastics. Furthermore, automation, manpower, skilled and proper collection management system should be steadfast through responsible government agencies. Significant R&D technology ramifications for anaerobic digestion, impurity eradication and waste recycling should be recommended through private and public agencies.

Conclusion

Polymeric sugars enmeshed in LCB can be obtained using the required pre-treatment method to transform them into biopolymers. Conversion of renewable chemicals generated from LCBs into biodegradable and recyclable plastic is an

entrancing option to supersede conventional petroleum-based plastics. Utilization of LCB for

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bioplastic production renders sustainability and promotes a circular economy, although variable structure, heterogenous nature and complexity of LCB are eloquent critical sides that need to be remediated through technological advancements and development of strategies for effective substrate conversion, which would directly enhance commercial viability. Bioplastic production from LCB is at an inchoate phase, but the future outlooks are promising and luring. Significant advancements in fermentation techniques with this inexpensive LCB have to potential to completely transform the shape of the biopolymer industry, allowing production costs to permit to an extent. It will compete with conventional plastic and will offer valuable biodegradable and biocompatible properties with environmental sustainability.

Conflict of interest

The authors declare that they have no conflict of interest.

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